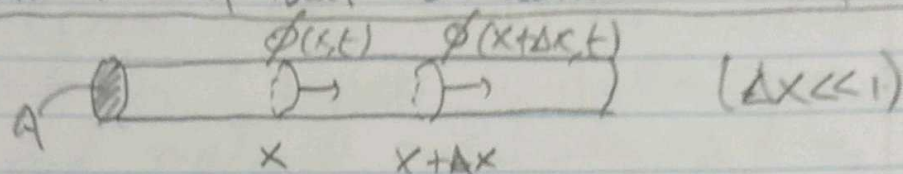


CHAPTER #1: HEAT EQ.1.2 | Derivation of heat conduction in a (quasi-) 1D rod

Def * $e(x, t) \equiv$ thermal energy density = heat density,

$$\Rightarrow \text{heat energy} = e(x, t) \cdot \text{Volume} = e(x, t) \cdot A \cdot \Delta x$$

* Energy (heat) conservation:

$$\frac{\partial}{\partial t} [e A \Delta x] \overset{\text{rate of change of heat energy}}{=} \underbrace{\text{heat lost/gained through boundaries}}_{\rightarrow \text{flux}} + \underbrace{\text{heat generated or lost inside Volume}}_{\rightarrow \text{sink/source}}$$

* Def: heat flux: $\phi(x) =$ thermal energy per unit time flowing to right per unit surface area

* Def: heat sources: $Q(x, t) =$ thermal energy per unit volume generated per unit time

$\rightarrow$ Inside the Δx -slice the total energy/time is $Q \cdot \text{Volume} = Q \cdot A \cdot \Delta x$
 $[\Delta x \text{ small so } Q(x) \approx \text{const}]$

Conservation: $\frac{\partial}{\partial t} [e A \Delta x] = \phi(x, t) \cdot A - \phi(x + \Delta x, t) \cdot A + Q A \cdot \Delta x$

$$\xRightarrow{\div A} \frac{\partial e}{\partial t} = \frac{\phi(x, t) - \phi(x + \Delta x, t)}{\Delta x} + Q$$

Now limit $\Delta x \rightarrow 0 \Rightarrow \boxed{\frac{\partial e}{\partial t} = -\frac{\partial \phi}{\partial x} + Q} \quad (1)$

We now need to relate $e \leftrightarrow \phi$

Temp. & specific heat.

Different materials behave differently: the same thermal energy might rise a specific ball of material by 2 degrees while the same ball made of $\neq$ material might only rise it by 1 degree...

- Def:
- $u(x,t) \equiv$ temperature
 - $c \equiv$ specific heat = heat energy necessary to raise the temp. of a unit mass by one temperature unit
 - $\rho(x) \equiv$ material density

∴ In the thin slice we have the energy:

$$\begin{aligned} e_{\Delta V} &= c \cdot u \cdot \text{mass} \\ &= c \cdot u \cdot \rho \cdot \Delta V \end{aligned} \quad \left. \vphantom{\begin{aligned} e_{\Delta V} &= c \cdot u \cdot \text{mass} \\ &= c \cdot u \cdot \rho \cdot \Delta V \end{aligned}} \right\} \boxed{e(x,t) = c \rho u(x,t)}$$

$$\stackrel{\textcircled{1}}{\Rightarrow} \frac{\partial e}{\partial t} = \frac{\partial}{\partial t} [c \rho u(x,t)] = -\frac{\partial \phi}{\partial x} + Q$$

material properties time independent $\left\{ \begin{array}{l} c \rightarrow c(x) \\ \rho \rightarrow \rho(x) \end{array} \right.$

$$\Rightarrow \boxed{c(x)\rho(x) \frac{\partial u}{\partial t} = -\frac{\partial \phi}{\partial x} + Q} \quad \textcircled{2}$$

Fourier's law [Equivalent to Hooke's law for springs]

→ relates temp $\leftrightarrow$ flux $[u \leftrightarrow \phi]$

Assume: 1) $u = \text{const} \Leftrightarrow \phi = 0$

2) ϕ flows from hotter $\rightarrow$ colder

3) higher temp difference $\rightarrow \phi \uparrow$

4) ϕ depends of material

3/

The simplest relation that satisfies 1)-4) is a linear relationship called Fourier's law of heat conduction:

$$\phi = -K_0 \frac{\partial u}{\partial x}$$

K_0 = material dependant (non-homogeneous material $\rightarrow K_0 = K_0(x)$)

$$\therefore c(x)g(x) \frac{\partial u}{\partial t} = -\frac{\partial}{\partial x} \left[K_0(x) \frac{\partial u}{\partial x} \right] + Q$$

Def: $k(x) \equiv K_0(x)/c(x)g(x)$

$$\Rightarrow \left[\frac{\partial u(x,t)}{\partial t} - k(x) \frac{\partial^2 u(x,t)}{\partial x^2} + \frac{Q(x,t)}{c(x)g(x)} \right] \quad (3)$$

For homogeneous material and NO sources/sinks

$$\rightarrow (4) \left[\frac{\partial u(x,t)}{\partial t} - k \frac{\partial^2 u(x,t)}{\partial x^2} \right] \quad \text{Heat Eq.}$$

$\rightarrow$ This eq. describes the DIFFUSION of heat. $\rightarrow$ Diffusion Eq.

$\rightarrow$ It is much more general as long as a similar version to Fourier's law applies for other systems:

- Diffusion of pollutants (see tut p 9-10)
- Diffusion of population
- etc, etc, ...

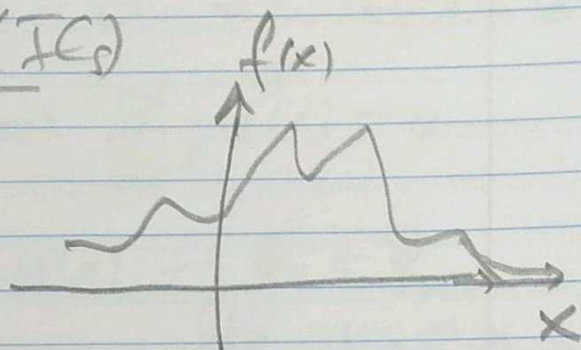
Vk of Diff. eq. relies on fluxes being proportional to gradients of the quantity being modelled.

PDE: $u_t = k u_{xx}$, $k > 0$, $u(x,t) \in \mathbb{R}$

ODE: BVP = ODE + IC
 Initial conditions.

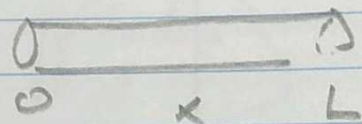
Initial conditions (IC)

$u(x, 0) = f(x)$
 $\uparrow_{t=0}$



Boundary conditions (BCs)

- * Infinite domain $x \in \mathbb{R}$
- * Finite domain $0 \leq x \leq L$



Temp. @ edges of rod:

prescribed
const.
temps.

Dirichlet BCs :

$$\begin{cases} u(x=0, t) = u_0 \\ u(x=L, t) = u_L \end{cases}$$

Neumann BCs :

$$\begin{cases} \frac{\partial u}{\partial x} \big|_{x=0, t} = -\phi_0/k_0 = A_0 \\ \frac{\partial u}{\partial x} \big|_{x=L, t} = -\phi_L/k_0 = A_L \end{cases}$$

and fixing flow rate @ boundaries.

1.4 Equilibrium temp. distribution

1.4.1 prescribed temp @ Boundaries (Dirichlet)

$$\text{IC: } \left[\begin{array}{l} u(x, 0) = f(x) \\ u(0, t) = T_1(t) \\ u(L, t) = T_2(t) \end{array} \right] + u_t = k u_{xx} \quad (4)$$

const. temp. @ Boundaries. $\begin{cases} T_1(t) = T_1 \\ T_2(t) = T_2 \end{cases}$

Q: What is the equil. temp. distribution?

A: $\rightarrow \frac{\partial u}{\partial t} = 0 \Rightarrow u(x,t) = u^*(x)$

Heat eq. $\Rightarrow \cancel{k u_{xx}} = 0 \Rightarrow \frac{\partial^2}{\partial x^2} u^*(x) = 0$

~~PDE~~ $\rightarrow$ ODE $u = u(x) \rightarrow \partial_x = \frac{d}{dx}$

$\Rightarrow \frac{d^2}{dx^2} u^*(x) = 0 \xRightarrow{\int dx} \frac{d}{dx} u^* = C_1$

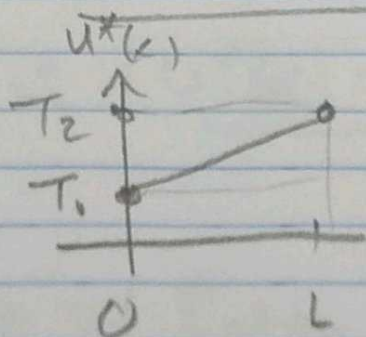
$\xRightarrow{\int dx} \underline{u^*(x) = C_1 x + C_2} \quad \parallel \text{Indep. of BCs}$

Use BCs $u^*(0) = T_1 \Rightarrow C_2 = T_1$

$u^*(L) = T_2 \Rightarrow C_1 L + C_2 = T_2$

$\Rightarrow C_1 = (T_2 - T_1)/L$

$\therefore \underline{u^*(x) = \frac{(T_2 - T_1)x}{L} + T_1}$

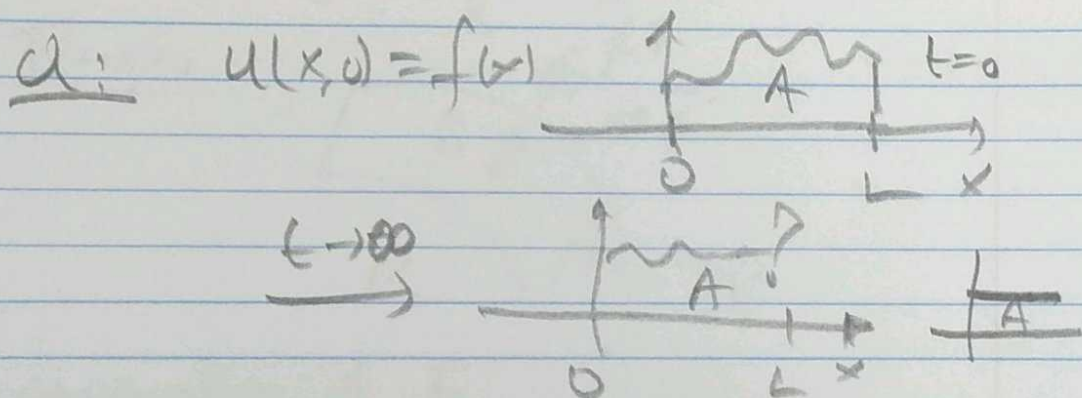


Eq. temp
for $u_t = k u_{xx}$
 $u(0,t) = T_1$
 $u(L,t) = T_2$
 ~~$u(x,0) = f(x)$~~

1.4.2 Insulated Boundaries.

Neumann BCs $\frac{\partial u(0,t)}{\partial x} = A_0$
 $\frac{\partial u(L,t)}{\partial x} = A_L$

$A_0 = A_L = 0 \Rightarrow$ No flux across boundaries
 $\rightarrow$ INSULATED.



Math: From b4 $u^*(x) = C_1 x + C_2$

BCs: $\frac{\partial u}{\partial x} = C_1$ $\begin{cases} x=0 \rightarrow \frac{\partial u}{\partial x}|_{x=0} = A_0 = 0 \Rightarrow C_1 = 0 \\ x=L \rightarrow \frac{\partial u}{\partial x}|_{x=L} = A_L = 0 \Rightarrow C_1 = 0 \end{cases}$

$C_1 = 0 \therefore \underline{u^*(x) = C_2}$ $\left[C_2 = \frac{1}{L} \int_0^L f(x) dx \right]$
 Physics.

Conservation of Energy

• Physics way $\rightarrow$ see textbook.

• Math: $u_t = k u_{xx} \xRightarrow{\int_0^L dx} \frac{\partial}{\partial t} \int_0^L u dx = \left[k u_x \right]_0^L$

$$\text{but } \left. \begin{array}{l} u_x(0,t) = 0 \\ u_x(L,t) = 0 \end{array} \right\} \text{ Insulated.}$$

$$\Rightarrow \frac{\partial}{\partial t} \int_0^L u(x,t) dx = 0$$

$$\Rightarrow \int_0^L u(x,t) dx = \text{const} = \underbrace{\int_0^L f(x) dx}_{u(0,t)}$$

$\therefore$ for equilibrium $u^* = C_2 -$

$$\Rightarrow \underbrace{\int_0^L u^* dx}_{\text{final}} = \underbrace{\int_0^L f(x) dx}_{\text{initial}}$$

$$\Rightarrow C_2 \int_0^L dx = \int_0^L f(x) dx$$

$$\Rightarrow \boxed{C_2 = \frac{1}{L} \int_0^L f(x) dx}$$

$\therefore$ If insulated boundaries and ARBITRARY initial temp. distribution $f(x)$

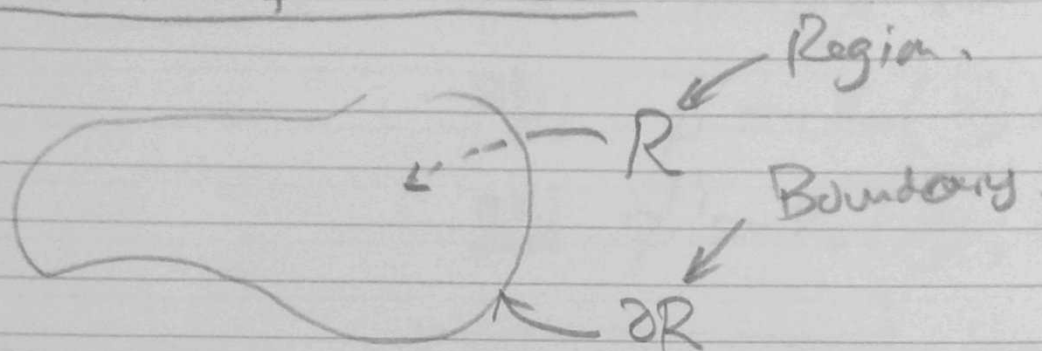
$$u(x,t) \xrightarrow{t \rightarrow \infty} u^*(x) = \frac{1}{L} \int_0^L f(x) dx$$



$$M = \text{"mass"} = \int_0^L u(x,t) dx$$

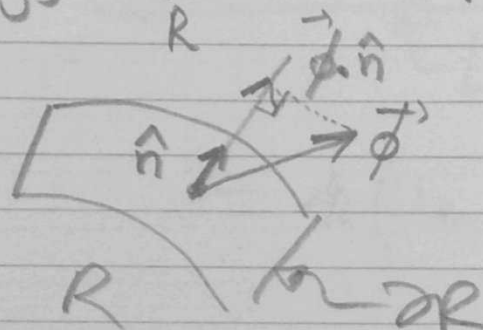
is a CONSERVED quantity in the heat (diffusion) eq. when INSULATED boundaries.

1.5 Heat eq. in 2D & 3D



• Total energy $\iiint_R e \, dv = \iiint_R c(\vec{r}) \rho(\vec{r}) u(\vec{r}, t) \, dv$

• Fluxes:



$$\vec{r} = (x, y, z)$$

• conservation of E

$$\frac{d}{dt} \iiint_R c \rho u \, dv - \oint_{\partial R} \vec{\phi} \cdot \hat{n} \, ds + \iiint_R Q \, dv = 0 \quad (5)$$

Divergence theo: $\nabla \cdot \vec{\phi} = \text{DEL}$

$$\begin{aligned} \text{Def: } \text{Div } \vec{\phi} &= \nabla \cdot \vec{\phi} = (\partial_x, \partial_y, \partial_z) \cdot (\phi_x, \phi_y, \phi_z) \\ &= \frac{\partial \phi_x}{\partial x} + \frac{\partial \phi_y}{\partial y} + \frac{\partial \phi_z}{\partial z} \end{aligned}$$

$$\text{Theo: } \iiint_R \nabla \cdot \vec{\phi} \, dv = \oint_{\partial R} \vec{\phi} \cdot \hat{n} \, ds$$

$$(5) \Rightarrow \iiint_R \left[c \rho \frac{\partial u}{\partial t} + \nabla \cdot \vec{\phi} - Q \right] = 0 \quad (6)$$

↑ Is true $\forall R \Rightarrow$ integrand = 0

Farries law

1D: $\phi = -K_0 \frac{\partial u}{\partial x}$

2D: $\vec{\phi} = -K_0 \left(\frac{\partial u}{\partial x}, \frac{\partial u}{\partial y} \right)$ (7)

3D: $\vec{\phi} = -K_0 \left(\frac{\partial u}{\partial x}, \frac{\partial u}{\partial y}, \frac{\partial u}{\partial z} \right)$

(7) + (6) $\Rightarrow$

$Q = 0$

↑ no sink
no sources

$\left[\frac{\partial u}{\partial t} = k \nabla^2 u \right]$ Heat eq.
in ND.

↑ Laplace. P.D.

$= k (u_{xx} + u_{yy} + u_{zz})$